

Viscosity Measurements on Gaseous Propane: Re-evaluation
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 DOI: 10.1021/je010062k]. Jörg Wilhelm and Eckhard Vogel*

Measurements of the viscosity (η) of propane by Wilhelm and Vogel, performed by means of a vibrating-wire viscometer with a freely suspended weight using measurements of temperature (T) and pressure (p) for the determination of the required density (ρ) with an older equation of state by Span and Wagner,¹ have been re-evaluated. The re-evaluation concerns the determination of the wire radius using an improved calibration as well as the calculation of the density by means of the recent equation of state by Lemmon et al.² The re-evaluated data are to be used together with new accurate ηppT data³ to test, particularly in the vicinity of the critical point, their performance in comparison with the viscosity surface correlation by Scalabrin et al.⁴

The recalibration of the old vibrating-wire viscometer was performed using a value for the radius of the wire that was newly determined using old measurements on argon⁵ and the currently accepted value for the zero-density viscosity coefficient of argon derived by Vogel et al.⁶ from an ab initio potential for argon on the basis of the kinetic theory of dilute gases ($\eta_{0,\text{Ar},298.15\text{K}} = 22.552 \mu\text{Pa}\cdot\text{s}$ with an uncertainty of $\pm 0.1\%$).

The results reported in Table 1 of the previous paper of Wilhelm and Vogel were restricted to ηpp triples along the measured isotherms. In this correction, we include more details about the re-evaluated measurements in order to make the information comparable to that given for the new ηppT measurements by Seibt et al.³ The individual points were not exactly measured at the nominal temperature of an isotherm (T_{nom}) but could be kept within small deviations. The experimental viscosity data were adjusted to $\eta_{T_{\text{nom}}}$ values at the nominal temperature using a Taylor series expansion restricted to the first power in temperature. For that purpose, the value of the temperature dependence for the low-density region, $(\partial\eta/\partial T)_{\rho} = (0.025 \text{ to } 0.027) \mu\text{Pa}\cdot\text{s}\cdot\text{K}^{-1}$, determined experimentally by Vogel⁷ for propane was used. Furthermore, it was assumed that the density values $\rho_{\text{eos}(T,p)}$ calculated from the measured values for T and p using the equation of state by Lemmon et al.² and those for the isotherms are the same. As a consequence, the pressures $p_{T_{\text{nom}},\rho_{\text{eos}}}$ at the nominal temperature changed and were recalculated from the densities. The corrected and improved experimental ηppT data from the earlier measurements of Wilhelm and Vogel on propane (seven isotherms at 298.15 K, 323.15 K, 348.15 K, 366.15 K, 373.15 K, 398.15 K, and 423.15 K) are summarized in Tables 1 to 7. It should be noted that some experimental points at the lowest densities could be influenced by the slip effect, and these values are marked in the tables.

The experimental results for each nominal isotherm for propane were correlated as a function of the reduced density ($\delta = \rho/\rho_{c,\text{C}_3\text{H}_8}$) by means of a power-series representation in which the highest power (n) was restricted to 6 or lower depending on the density range and the reduced temperature ($\tau = T/T_{c,\text{C}_3\text{H}_8}$):

Table 1. Corrected Experimental ηppT Data for Propane at 298.15 K

T	p	$p_{298.15\text{K},\rho_{\text{eos}}}$	$\rho_{\text{eos}(T,p)}$	η	$\eta_{298.15\text{K}}$
K	MPa	MPa	$\text{kg}\cdot\text{m}^{-3}$	$\mu\text{Pa}\cdot\text{s}$	$\mu\text{Pa}\cdot\text{s}$
298.21	0.039382	0.039374	0.70478	8.116 ^a	8.114 ^a
298.21	0.066942	0.066929	1.2033	8.119	8.117
298.21	0.093547	0.093528	1.6889	8.120	8.118
298.19	0.11053	0.11051	2.0012	8.118	8.117
298.21	0.12184	0.12182	2.2100	8.118	8.117
298.20	0.13585	0.13583	2.4700	8.117	8.116
298.21	0.15473	0.15470	2.8221	8.118	8.116
298.20	0.16719	0.16716	3.0559	8.117	8.116
298.18	0.17777	0.17775	3.2554	8.118	8.117
298.21	0.18944	0.18940	3.4756	8.115	8.114
298.21	0.20013	0.20008	3.6784	8.117	8.116
298.18	0.20911	0.20908	3.8499	8.116	8.115
298.21	0.22444	0.22439	4.1427	8.115	8.113
298.18	0.23895	0.23893	4.4224	8.116	8.115
298.21	0.25229	0.25223	4.6796	8.116	8.114
298.18	0.26413	0.26410	4.9102	8.114	8.113
298.21	0.28129	0.28123	5.2447	8.116	8.114
298.18	0.29872	0.29869	5.5879	8.115	8.115
298.18	0.33908	0.33904	6.3899	8.116	8.115
298.21	0.35154	0.35146	6.6393	8.116	8.115
298.18	0.36020	0.36016	6.8148	8.112	8.111
298.19	0.39256	0.39250	7.4721	8.117	8.116
298.19	0.42870	0.42864	8.2171	8.117	8.116
298.19	0.46202	0.46194	8.9138	8.118	8.117
298.19	0.49882	0.49874	9.6951	8.121	8.120
298.19	0.53009	0.53000	10.369	8.123	8.122
298.19	0.56644	0.56635	11.165	8.126	8.125
298.20	0.60516	0.60503	12.026	8.129	8.128
298.19	0.63960	0.63949	12.808	8.132	8.131
298.19	0.67731	0.67719	13.678	8.135	8.134
298.18	0.71567	0.71557	14.582	8.141	8.140
298.19	0.75229	0.75215	15.461	8.146	8.145
298.19	0.78826	0.78812	16.342	8.151	8.150
298.20	0.82490	0.82471	17.259	8.158	8.156
298.20	0.85910	0.85890	18.133	8.165	8.164
298.19	0.91615	0.91597	19.637	8.176	8.175

^a Influenced by slip.

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Table 3. Continued

<i>T</i>	<i>p</i>	$p_{348.15K,\rho_{eos}}$	$\rho_{eos(T,p)}$	η	$\eta_{348.15K}$
K	MPa	MPa	$\text{kg}\cdot\text{m}^{-3}$	$\mu\text{Pa}\cdot\text{s}$	$\mu\text{Pa}\cdot\text{s}$
348.15	2.1859	2.1859	45.364	10.140	10.140
348.15	2.2450	2.2450	47.233	10.188	10.188
348.15	2.3255	2.3255	49.902	10.259	10.259
348.15	2.3933	2.3933	52.269	10.322	10.322
348.15	2.4585	2.4585	54.669	10.393	10.393
348.15	2.5270	2.5270	57.339	10.473	10.473
348.15	2.5891	2.5891	59.918	10.556	10.556
348.15	2.6553	2.6553	62.856	10.650	10.650
348.15	2.7010	2.7010	65.022	10.722	10.722
348.14	2.7313	2.7314	66.542	10.774	10.774

^aInfluenced by slip.**Table 4. Continued**

<i>T</i>	<i>p</i>	$p_{366.15K,\rho_{eos}}$	$\rho_{eos(T,p)}$	η	$\eta_{366.15K}$
K	MPa	MPa	$\text{kg}\cdot\text{m}^{-3}$	$\mu\text{Pa}\cdot\text{s}$	$\mu\text{Pa}\cdot\text{s}$
366.14	0.69712	0.69714	10.742	9.999	9.999
366.14	0.75126	0.75128	11.637	10.009	10.010
366.16	0.75559	0.75557	11.708	10.007	10.007
366.14	0.82041	0.82044	12.794	10.025	10.025
366.16	0.84809	0.84806	13.261	10.027	10.026
366.14	0.84914	0.84917	13.280	10.029	10.029
366.15	0.88069	0.88069	13.816	10.039	10.039
366.15	0.95539	0.95539	15.101	10.048	10.048
366.15	0.98588	0.98588	15.632	10.056	10.056
366.15	1.0298	1.0298	16.402	10.065	10.065
366.15	1.0979	1.0979	17.613	10.085	10.085
366.15	1.1362	1.1362	18.301	10.094	10.094
366.15	1.1708	1.1708	18.928	10.103	10.103
366.15	1.2452	1.2452	20.295	10.125	10.125
366.15	1.3048	1.3048	21.407	10.142	10.142
366.12	1.3621	1.3623	22.496	10.159	10.160
366.12	1.4287	1.4288	23.776	10.182	10.183
366.12	1.4940	1.4942	25.054	10.206	10.207
366.12	1.5640	1.5642	26.449	10.232	10.233
366.12	1.6327	1.6329	27.844	10.257	10.258
366.12	1.6943	1.6945	29.117	10.283	10.284
366.13	1.7509	1.7510	30.304	10.308	10.309
366.14	1.8632	1.8633	32.725	10.359	10.360
366.14	1.9236	1.9237	34.062	10.388	10.388
366.14	1.9775	1.9776	35.277	10.415	10.415
366.14	2.0473	2.0473	36.882	10.450	10.450
366.14	2.1247	2.1248	38.709	10.496	10.497
366.14	2.1774	2.1774	39.980	10.526	10.526
366.12	2.2195	2.2198	41.020	10.553	10.554
366.11	2.3138	2.3142	43.399	10.609	10.611
366.11	2.3705	2.3709	44.871	10.653	10.654
366.12	2.4406	2.4409	46.735	10.705	10.706
366.12	2.5104	2.5108	48.653	10.758	10.758
366.13	2.5693	2.5695	50.312	10.806	10.806
366.13	2.6227	2.6230	51.862	10.850	10.851
366.14	2.6980	2.6982	54.109	10.921	10.921
366.15	2.7596	2.7596	56.011	10.974	10.974
366.15	2.8306	2.8306	58.286	11.049	11.049
366.15	2.9194	2.9194	61.269	11.145	11.145
366.15	2.9806	2.9806	63.419	11.215	11.215
366.13	3.0484	3.0488	65.917	11.305	11.305
366.12	3.1078	3.1084	68.200	11.393	11.394
366.13	3.1714	3.1718	70.743	11.478	11.479
366.08	3.2574	3.2588	74.449	11.620	11.621
366.10	3.3142	3.3153	77.010	11.713	11.714
366.10	3.3670	3.3681	79.537	11.825	11.827
366.15	3.4159	3.4159	81.939	11.921	11.921
366.15	3.4846	3.4846	85.635	12.077	12.077
366.15	3.5441	3.5441	89.107	12.223	12.223
366.15	3.5974	3.5974	92.472	12.382	12.382
366.19	3.6427	3.6415	95.489	12.530	12.529
366.13	3.6903	3.6909	99.157	12.697	12.697
366.15	3.7038	3.7038	100.17	12.762	12.762
366.16	3.7483	3.7480	103.90	12.933	12.933
366.18	3.7977	3.7967	108.52	13.166	13.165
366.19	3.8343	3.8328	112.42	13.361	13.360

Table 4. Continued

<i>T</i>	<i>p</i>	$p_{366.15K,\rho_{eos}}$	$\rho_{eos(T,p)}$	η	$\eta_{366.15K}$
K	MPa	MPa	$\text{kg}\cdot\text{m}^{-3}$	$\mu\text{Pa}\cdot\text{s}$	$\mu\text{Pa}\cdot\text{s}$
366.20	3.8694	3.8675	116.68	13.585	13.584

^aInfluenced by slip.**Table 5. Continued**

<i>T</i>	<i>p</i>	$p_{373.15K,\rho_{eos}}$	$\rho_{eos(T,p)}$	η	$\eta_{373.15K}$
K	MPa	MPa	$\text{kg}\cdot\text{m}^{-3}$	$\mu\text{Pa}\cdot\text{s}$	$\mu\text{Pa}\cdot\text{s}$
373.13	2.0041	2.0043	34.612	10.631	10.631
373.13	2.0877	2.0879	36.439	10.675	10.676
373.13	2.1522	2.1524	37.881	10.709	10.710
373.14	2.2204	2.2204	39.433	10.746	10.746
373.14	2.2810	2.2811	40.845	10.781	10.781
373.10	2.3457	2.3462	42.392	10.820	10.821
373.10	2.4275	2.4280	44.386	10.874	10.876
373.10	2.4697	2.4702	45.437	10.901	10.903
373.09	2.5473	2.5480	47.417	10.955	10.957
373.09	2.6046	2.6053	48.913	10.997	10.998
373.08	2.6766	2.6775	50.845	11.055	11.057
373.08	2.7500	2.7509	52.868	11.108	11.110
373.08	2.8397	2.8407	55.431	11.190	11.192
373.08	2.8799	2.8810	56.612	11.229	11.231
373.09	2.9419	2.9428	58.472	11.289	11.290
373.09	3.0147	3.0156	60.733	11.367	11.368
373.10	3.0773	3.0781	62.739	11.430	11.432
373.11	3.1412	3.1419	64.857	11.504	11.505
373.12	3.2312	3.2317	67.970	11.614	11.614
373.12	3.2899	3.2904	70.095	11.698	11.699
373.17	3.3525	3.3521	72.415	11.778	11.778
373.19	3.4214	3.4205	75.098	11.884	11.883
373.20	3.4841	3.4830	77.665	11.988	11.986
373.20	3.5585	3.5574	80.884	12.113	12.111
373.21	3.6575	3.6560	85.467	12.317	12.315
373.12	3.7420	3.7428	89.860	12.514	12.515
373.11	3.8069	3.8080	93.419	12.666	12.667
373.10	3.8668	3.8682	96.955	12.835	12.837
373.10	3.9578	3.9594	102.85	13.125	13.126
373.10	4.0432	4.0449	109.15	13.440	13.442
373.11	4.1489	4.1505	118.43	13.949	13.950
373.12	4.2121	4.2134	125.12	14.343	14.344
373.14	4.2866	4.2871	134.79	14.898	14.898
373.06	4.3708	4.3755	151.30	15.982	15.984
373.12	4.3982	4.3999	157.71	16.359	16.360
373.08	4.4249	4.4291	167.53	17.183	17.185
373.12	4.4384	4.4403	172.24	17.351	17.352
373.12	4.4600	4.4619	183.76	18.274	18.275
373.10	4.4661	4.4695	188.76	18.567	18.568
373.11	4.4787	4.4816	198.17	19.205	19.206
373.10	4.4991	4.5030	218.37	21.060	21.061
373.10	4.5126	4.5167	231.22	22.480	22.482
373.15	4.5286	4.5286	240.76	23.633	23.633
373.11	4.5401	4.5437	250.41	24.999	25.000
373.12	4.5655	4.5684	261.77	26.823	26.823
373.17	4.5838	4.5818	266.46	27.481	27.481
373.12	4.5911	4.5942	270.15	28.087	28.087
373.12	4.6414	4.6447	281.48	29.839	29.840
373.13	4.6975	4.6999	290.07	31.300	31.300
373.14	4.7421	4.7433	295.36	32.198	32.198
373.17	4.8610	4.8583	305.94	34.022	34.021
373.08	4.9512	4.9609	313.00	35.311	35.313
373.08	5.0513	5.0614	318.68	36.361	36.363

Table 8. Coefficients of Equation 1 for the Re-evaluated Viscosity Measurements on Propane

T K	n	ρ_{\max} $\text{kg}\cdot\text{m}^{-3}$	η_0	η_1	η_2	η_3	η_4	η_5	η_6	σ
			$\mu\text{Pa}\cdot\text{s}$							
298.15	2	20.48	8.122 ± 0.001	-0.689 ± 0.029	14.445 ± 0.317					0.012
323.15	2	38.26	8.787 ± 0.001	0.073 ± 0.025	13.595 ± 0.151					0.021
348.15	3	70.64	9.436 ± 0.001	0.910 ± 0.023	13.370 ± 0.197	-5.732 ± 0.454				0.018
366.15	3	116.68	9.907 ± 0.001	1.300 ± 0.019	12.107 ± 0.101	-2.675 ± 0.140				0.030
373.15	6	447.05	10.090 ± 0.001	1.716 ± 0.025	11.764 ± 0.180	-6.092 ± 0.470	7.765 ± 0.511	-3.993 ± 0.245	0.980 ± 0.043	0.027
398.15	6	416.76	10.743 ± 0.001	1.801 ± 0.027	13.969 ± 0.176	-10.536 ± 0.444	10.920 ± 0.510	-4.905 ± 0.269	1.061 ± 0.053	0.035
423.15	6	380.08	11.370 ± 0.001	2.192 ± 0.031	13.610 ± 0.213	-9.894 ± 0.576	10.274 ± 0.712	-4.764 ± 0.405	1.089 ± 0.086	0.033

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